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# An equation of state applied to sodium chloride and caesium chloride at high pressures and high temperatures 

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#### Abstract

In the present paper, an equation of state is proposed which has been found to be applicable at high pressures and high temperatures. The proposed equation of state has been used to compute the pressure-volume behaviour, the isothermal bulk modulus and its pressure derivative, the coefficient of thermal expansion and the Anderson-Grüneisen parameter of NaCl and CsCl at high pressures (up to 400 kbar ) and high temperatures (up to 1073 K ). The results obtained for $V(P, T) / V(0, T)$ are found to be in very good agreement with Decker's data in the whole ranges of pressure and temperature. Further, the other calculated results are also found to be in good agreement with the experimental data. The present calculations definitely lend support to the proposed equation of state and to the method used to extend the applicability at higher temperatures.


## 1. Introduction

In principle, all the thermodynamic properties of a system can be predicted once precise knowledge of the interatomic forces becomes known, but the imprecise knowledge of the interatomic forces along with the limitations of the procedure to carry through the prediction compel us to use simplifying models and approximations to obtain an equation of state. In support of the statement, some examples can be given here: the equations of state obtained by Murnaghan (1949, 1951), Keane (1954) and Birch (1952).

With the advancement in high-pressure physics, there has been extensive experimental and theoretical work to determine the equation of state. However, even for a simple substance such as sodium chloride a reliable theoretical equation of state cannot be predicted owing to lack of precise knowledge of the interatomic potential. Moreover, the results depend strongly on the kind of model and the input data used for calculation.

Therefore the purpose of the present paper is
(i) to propose an equation of state which is applicable to high pressures and
(ii) to calculate the isothermal bulk modulus and its pressure derivative along with the Anderson-Grüneisen parameter and coefficient of thermal expansion at various pressures (up to 400 kbar ) and at elevated temperatures (up to 1073 K ).

To apply the proposed equation of state, we choose solid sodium chloride and caesium chloride because extensive compression data for both these solids have been given by Decker (1971). Moreover, sodium chloride is widely used as an internal pressure standard in high-pressure x-ray studies.

## 2. Theory

To obtain the equation of state, we assume that the ratio of second to first pressure derivatives of the isothermal bulk modulus $B_{T}(P, T)$ is a pressure-independent quantity, i.e.

$$
\begin{equation*}
\left.\left[\partial^{2} B_{T}(P, T) / \partial P^{2}\right)\right]_{T} /\left[\partial B_{T}(P, T) / \partial P\right]_{T}=-Z \tag{1}
\end{equation*}
$$

The successive integration of equation (1) within the limits $P=0$ and $P=P$ give the following equations:

$$
\begin{align*}
& B_{T}^{\prime}(P, T)=B_{T}^{\prime}(0, T) \exp (-Z P)  \tag{2}\\
& B_{T}(P, T)=B_{T}(0, T)+\left[B_{T}^{\prime}(0, T) / Z\right][1-\exp (-Z P)] \tag{3}
\end{align*}
$$

and
$\ln [V(P, T) / V(0, T)]=-(1 / \eta) \ln \left\{1+\left[B_{T}^{\prime}(0, T) / B_{T}(0, T) Z\right][1-\exp (-Z P)]\right\}-Z P / \eta$
where $\eta=B_{T}(0, T) Z+B_{T}^{\prime}(0, T)$ and $B_{T}^{\prime}(0, T)$ is the first pressure derivative of bulk modulus $B_{T}(0, T)$ at $P=0$.

The following results can be easily obtained from equations (1)-(4).
(i) The volume decreases continuously with increasing pressure and becomes zero as the pressure tends to infinity.
(ii) The bulk modulus $B_{T}=-V(\partial P / \partial V)_{T}$ increases continuously with increasing pressure and has a finite value equal to $\left[B_{T}(0, T)+B_{T}^{\prime}(0, T) / Z\right]$ as $P \rightarrow \infty$. This is totally a new result which is obtained here.
(iii) The first pressure derivative $\left(\partial B_{T}(P, T) / \partial P\right)_{T}$ of the bulk modulus decreases with increasing pressure and therefore the second derivative of $B_{T}(P, T)$ is negative.
(iv) Under the condition that $Z$ is very small, equation (4) can be easily transformed to the well known equation of Murnaghan $(1949,1951)$.
(v) It is interesting that equation (1) has a general form which is given as

$$
\begin{equation*}
\left[\partial^{n} B_{T}(P, T) / \partial P^{n}\right]_{T} /\left[\partial B_{T}(P, T) / \partial P\right]_{T}=(-1)^{n-1} Z^{n-1} \tag{5}
\end{equation*}
$$

where $n$ is the order of derivative.
The first three results are the same as obtained from the experiments (Spetzler et al 1972). Result (iv) suggests that the Murnaghan equation is a special case of the present equation of state. Result ( v ) suggests that the higher pressure derivative of bulk modulus can be obtained easily once the value of $Z$ and $\left[\partial B_{T}(P, T) / \partial P\right]_{T}$ become known.

Further, to minimise the adjustable parameters and to have a wide range applicability of the present equation of state, we assume the following.
(a) $B_{T}^{\prime}(0, T)$ and $Z$ are temperature-independent quantities, i.e.

$$
\begin{equation*}
\left(\partial B_{T}^{\prime} / \partial T\right)_{P}=0 \tag{6a}
\end{equation*}
$$

and

$$
\begin{equation*}
(\partial Z / \partial T)_{P}=0 \tag{6b}
\end{equation*}
$$

(b) The bulk modulus is a linear function of temperature, i.e.

$$
\begin{equation*}
B_{T}(0, T)=B_{T}\left(0, T_{0}\right)-\left(\partial B_{T} / \partial T\right)_{0}\left(T-T_{0}\right) . \tag{7}
\end{equation*}
$$

In equations (6) and (7), $T_{0}$ is some reference temperature at which $B_{T}\left(0, T_{0}\right)$ is
known and $\left(\partial B_{T} / \partial T\right)_{0}$ is the temperature derivative of the bulk modulus at $P=0$. Putting equations (6) and (7) into equation (3), we get
$B_{T}(P, T)=\left[B_{T}\left(0, T_{0}\right)-\left(\partial B_{T} / \partial T\right)_{0}\left(T-T_{0}\right)\right]+\left[B_{T}^{\prime}(0, T) / Z\right][1-\exp (-Z P)]$.
Further, to compare the results of $V(P, T) / V(0, T)$ obtained from the proposed equation of state with other equations, we use the following equations:

$$
\begin{equation*}
V(P, T) / V(0, T)=1-a\left[1-(1+b P)^{-c}\right] \tag{9}
\end{equation*}
$$

and

$$
\begin{equation*}
V(P, T) / V(0, T)=\left[1-a^{\prime} \ln \left(1+b^{\prime} P\right)\right]^{c^{\prime}} \tag{10}
\end{equation*}
$$

where

$$
\begin{aligned}
& a=\left(1+B_{0}^{\prime}\right) /\left(1+B_{0}^{\prime}+B_{0} B_{0}^{\prime \prime}\right) \\
& b=B_{0}^{\prime} / B_{0}-B_{0}^{\prime \prime} /\left(1+B_{0}^{\prime}\right) \\
& c=\left(1+B_{0}^{\prime}+B_{0} B_{0}^{\prime \prime}\right) /\left(B_{0}^{\prime 2}+B_{0}^{\prime}-B_{0} B_{0}^{\prime \prime}\right) \\
& a^{\prime}=\left[\left(B_{0}^{\prime 2}-4 B_{0} B_{0}^{\prime \prime}\right)^{1 / 2}\right] /\left[\left(B_{0}^{\prime 2}-4 B_{0} B_{0}^{\prime \prime}\right)^{1 / 2}+B_{0}^{\prime}\right] \\
& b^{\prime}=\left[\left(B_{0}^{\prime 2}-4 B_{0} B_{0}^{\prime \prime}\right)^{1 / 2}+B_{0}^{\prime}\right] / 2 B_{0} \\
& c^{\prime}=2 /\left[\left(B_{0}^{\prime 2}-4 B_{0} B_{0}^{\prime \prime}\right)^{1 / 2}+B_{0}^{\prime}\right] \\
& B_{0}=B_{T}(0, T) \quad B_{0}^{\prime}=B_{T}^{\prime}(0, T) \quad B_{0}^{\prime \prime}=B_{T}^{\prime \prime}(0, T)
\end{aligned}
$$

Equation (9) is given by Huang and Chow (1974) while equation (10) is given by Freund and Ingalls (1989).

We are using these equations for comparison because they are useful for higherpressure EXAFs work in which one has to express $r / r_{0}$ as a function of pressure which is just the third root of $V(P, T) / V(0, T)$ in equations (4), (9) and (10). Here $r$ is the distance between two atoms, e.g. the nearest neighbours.

## 3. Calculations and results

Thus the volume, bulk modulus and its pressure derivative and other thermodynamic properties can be easily calculated once the four adjustable parameters $B_{T}\left(0, T_{0}\right)$, $B_{T}^{\prime}\left(0, T_{0}\right), Z$ and $\left(\partial B_{T} / \partial T\right)_{0}$ become known. The three parameters $B_{T}\left(0, T_{0}\right)$, $B_{T}^{\prime}\left(0, T_{0}\right)$ and $Z$ become known once Decker's (1971) compression data at $T_{0}=25^{\circ} \mathrm{C}$ are fitted with equations (4), (9) and (10). The values of $B_{T}\left(0, T_{0}\right), B_{T}^{\prime}\left(0, T_{0}\right)$ and $Z$ along with the root mean square deviations are reported in table 1 . Thus, it is clear from table 1 that the proposed equation of state is better than the other two equations of state used here.

Further, the values of $\left(\partial B_{T} / \partial T\right)_{0}$ are obtained by fitting the compression data at other temperatures in the case of proposed equation of state. The values of the parameter so obtained are also reported in table 1.

### 3.1. Compression studies

By making use of equation (4) and taking the values of the parameters from table 1 , the values of $V(P, T) / V(0, T)$ are calculated as a function of pressure at different temperatures. For comparison, the calculated and Decker's values are reported in tables 2 and 3 at $25^{\circ} \mathrm{C}$ for sodium chloride and caesium chloride, respectively. At other
Table 1. Input data used.

| Equation used | Solid | $\begin{aligned} & T_{0} \\ & (\mathrm{~K}) \end{aligned}$ | $\begin{aligned} & B_{\tau}\left(0, T_{0}\right) \\ & \text { (kbar) } \end{aligned}$ | $\begin{aligned} & B_{T}^{\prime}\left(0, T_{0}\right) \\ & (\mathrm{kbar}) \end{aligned}$ | $\begin{aligned} & Z \times 10^{3} \\ & \left(\text { kbar }^{-1}\right) \end{aligned}$ | RMS deviation $\left(10^{-4}\right)$ | $\begin{aligned} & \left(\partial B_{T} / \partial T\right)_{0} \times 10^{2} \\ & \left(\operatorname{kbar} K^{-1}\right) \end{aligned}$ | $\begin{aligned} & \alpha\left(0, T_{0}\right) \times 10^{4} \\ & \left(\mathrm{~K}^{-1}\right) \end{aligned}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Equation (4) | NaCl | 298 | 240.14 | 4.54 | 1.236 | 1.56 | 12.37 | 1.1752 |
| Proposed equation | CsCl | 298 | 172.51 | 4.96 | 1.306 | 3.79 | 11.24 | - |
| Equation (9) | NaCl | 298 | 239.98 | 4.721 | 2.872 | 2.44 | - | - |
| (Proposed equation) | CsCl | 298 | 170.72 | 5.283 | 4.217 | 5.22 | - | - |
| Equation (10) | NaCl | 298 | 239.19 | 4.745 | 3.140 | 2.15 | - | - |
| (Proposed equation) | CsCl | 298 | 170.44 | 5.322 | 4.660 | 4.30 | - | - |



Figure 1. Variation in $V(P, T) / V(0, T)$ with pressure for NaCl at different temperatures: ——, calculated; . . . ., Decker's data.
temperatures, a comparison is shown in figures 1 and 2 . For the whole range of pressures and temperatures, the agreement is very good, particularly where the uncertainties in Decker's results which is $1.1 \%$ below $50 \mathrm{kbar}, 1.7 \%$ below 100 kbar and $2.4 \%$ below 200 kbar are taken into account.

Further, it is appropriate to mention here that the accuracies of Decker's results are comparable with the experimental capability. To validate this statement, we calculate $V(P, T) / V(0, T)$ at $25^{\circ} \mathrm{C}$ for sodium chloride from the proposed equation of state taking the values of the parameters from table 1 at the pressures used by Liu et al (1970). The calculated and the experimental results are reported in table 4 . The agreement is very good which indicates the correctness of the statement. The error in volume data of Liu et al (1970) is $\pm 0.45 \%$.

### 3.2. Bulk modulus and its first pressure derivative

The isothermal bulk modulus and its first pressure derivative can be easily obtained with the help of equations (3) and (2), respectively, by making use of the parameters from table 1 .

The calculated values of $B_{T}(P, T)$ as a function of pressure at different temperatures for both the solids are reported in figures 3 and 4. However, the variation in $B_{T}^{\prime}(P, T)$ as a function of pressure at $25^{\circ} \mathrm{C}$ is reported in figure 5 . It is clear from figures 3 and 4 that $B_{T}(P, T)$ does not increase linearly with pressure as is assumed in case of the Murnaghan $(1949,1951)$ equation.

However, the curves in figures 3 and 4 appear to indicate that it is possible to divide these curves into segments in which $B_{T}(P, T)$ varies linearly with pressure. A similar conclusion can also be drawn for $B_{T}^{\prime}(P, T)$.

It will be interesting to compare calculated values of $B_{T}(P, T)$ with the experimental data. For this purpose, we report the calculated and the experimental data (Spetzler et al 1972) on $B_{T}(P, T)$ for sodium chloride in the pressure range $0-30 \mathrm{kbar}$ at 300 K in table 5. The agreement is good. However, it may be mentioned here that the calculated values of $B_{T}(P, T)$ at 550 and 800 K are found to be higher than the experimental values (Spetzler et al 1972).

Table 2. $V(P, T) / V(0, T)$ as a function of pressure for sodium chloride at $25^{\circ} \mathrm{C}$.

| Sample No. | $\begin{aligned} & P \\ & \text { (kbar) } \end{aligned}$ | $V(P, T) / V(0, T)$ |  | Sample No. | $\begin{aligned} & P \\ & \text { (kbar) } \end{aligned}$ | $V(P, T) / V(0, T)$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | Decker's data | Calculated |  |  | Decker's data | Calculated |
| 1 | 1.44 | 0.9940 | 0.9941 | 36 | 91.89 | 0.7992 | 0.7990 |
| 2 | 2.94 | 0.9980 | 0.9881 | 37 | 96.04 | 0.7940 | 0.7939 |
| 3 | 4.47 | 0.9821 | 0.9823 | 38 | 100.31 | 0.7889 | 0.7888 |
| 4 | 6.06 | 0.9762 | 0.9764 | 39 | 104.69 | 0.7838 | 0.7837 |
| 5 | 7.70 | 0.9703 | 0.9705 | 40 | 109.21 | 0.7787 | 0.7786 |
| 6 | 9.38 | 0.9644 | 0.9648 | 41 | 113.84 | 0.7736 | 0.7736 |
| 7 | 11.12 | 0.9586 | 0.9588 | 42 | 118.61 | 0.7686 | 0.7685 |
| 8 | 12.91 | 0.9528 | 0.9530 | 43 | 123.52 | 0.7636 | 0.7635 |
| 9 | 14.76 | 0.9470 | 0.9472 | 44 | 128.55 | 0.7586 | 0.7586 |
| 10 | 16.67 | 0.9412 | 0.9414 | 45 | 133.73 | 0.7536 | 0.7536 |
| 11 | 18.63 | 0.9354 | 0.9356 | 46 | 139.06 | 0.7486 | 0.7487 |
| 12 | 20.65 | 0.9297 | 0.9299 | 47 | 144.53 | 0.7437 | 0.7437 |
| 13 | 22.74 | 0.9240 | 0.9241 | 48 | 150.15 | 0.7388 | 0.7387 |
| 14 | 24.88 | 0.9183 | 0.9185 | 49 | 155.93 | 0.7339 | 0.7340 |
| 15 | 27.10 | 0.9127 | 0.9128 | 50 | 161.87 | 0.7290 | 0.7291 |
| 16 | 29.37 | 0.9070 | 0.9071 | 51 | 167.97 | 0.7242 | 0.7243 |
| 17 | 31.72 | 0.9014 | 0.9015 | 52 | 174.25 | 0.7193 | 0.7195 |
| 18 | 34.13 | 0.8958 | 0.8959 | 53 | 180.69 | 0.7145 | 0.7147 |
| 19 | 36.62 | 0.8903 | 0.8903 | 54 | 187.31 | 0.7097 | 0.7099 |
| 20 | 39.18 | 0.8847 | 0.8847 | 55 | 194.12 | 0.7050 | 0.7051 |
| 21 | 41.82 | 0.8792 | 0.8791 | 56 | 201.11 | 0.7002 | 0.7004 |
| 22 | 44.53 | 0.8737 | 0.8736 | 57 | 208.29 | 0.6955 | 0.6957 |
| 23 | 47.32 | 0.8683 | 0.8682 | 58 | 215.67 | 0.6908 | 0.6910 |
| 24 | 50.20 | 0.8628 | 0.8627 | 59 | 223.26 | 0.6861 | 0.6863 |
| 25 | 53.16 | 0.8574 | 0.8572 | 60 | 231.05 | 0.6815 | 0.6816 |
| 26 | 56.20 | 0.8520 | 0.8518 | 61 | 239.05 | 0.6768 | 0.6769 |
| 27 | 59.33 | 0.8466 | 0.8464 | 62 | 247.27 | 0.6722 | 0.6723 |
| 28 | 62.55 | 0.8412 | 0.8411 | 63 | 255.72 | 0.6676 | 0.6677 |
| 29 | 65.87 | 0.8359 | 0.8357 | 64 | 264.39 | 0.6631 | 0.6631 |
| 30 | 69.28 | 0.8306 | 0.8304 | 65 | 273.31 | 0.6585 | 0.6584 |
| 31 | 72.79 | 0.8253 | 0.8251 | 66 | 282.46 | 0.6540 | 0.6539 |
| 32 | 76.40 | 0.8200 | 0.8198 | 67 | 291.87 | 0.6495 | 0.6493 |
| 33 | 80.11 | 0.8148 | 0.8146 | 68 | 301.53 | 0.6450 | 0.6447 |
| 34 | 83.93 | 0.8096 | 0.8094 | 69 | 311.45 | 0.6405 | 0.6401 |
| 35 | 87.85 | 0.8044 | 0.8042 |  |  |  |  |

### 3.3. Thermal coefficient

It will be really interesting to study the coefficient of thermal expansion as a function of pressure. For this purpose we use the idea given by Dass and Kumari (1984). They have pointed out that the product of the measured isothermal bulk modulus $B_{T}(P, T)$ and the thermal expansion coefficient $\alpha(P, T)$, is approximately independent of pressure:

$$
\begin{equation*}
\alpha(P, T) B_{T}(P, T)=\alpha(0, T) B_{T}(0, T)=\varepsilon(T) \tag{11}
\end{equation*}
$$

Equation (11) has also been shown to be valid at least to a good approximation by Swenson (1968), Yagi (1978) and Boehler and Kennedy (1980a). Putting the value of $B_{T}(P, T)$ from equation (3) into equation (11), we get $\alpha(P, T)=\alpha(0, T)\left\{1+\left(B_{T}^{\prime}(0, T) / B_{T}(0, T) Z\right)[1-\exp (-Z P)]\right\}^{-1}$.
Thus, equation (12) can be used to determine $\alpha(P, T)$ as a function of pressure.

Table 3. $V(P, T) / V(0, T)$ as a function of pressure for caesium chloride at $25^{\circ} \mathrm{C}$.

| No. | $\begin{aligned} & P \\ & (\text { kbar }) \end{aligned}$ | $V(P, T) / V(0, T)$ |  | No. | $\begin{aligned} & P \\ & \text { (kbar) } \end{aligned}$ | $V(P, T) / V(0, T)$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | Decker's data | Calculated |  |  | Decker's data | Calculated |
| 1 | 2.08 | 0.9880 | 0.9883 | 22 | 99.71 | 0.7586 | 0.7582 |
| 2 | 4.32 | 0.9762 | 0.9767 | 23 | 108.29 | 0.7486 | 0.7483 |
| 3 | 6.72 | 0.9644 | 0.9650 | 24 | 117.40 | 0.7388 | 0.7386 |
| 4 | 9.29 | 0.9528 | 0.9534 | 25 | 127.07 | 0.7290 | 0.7289 |
| 5 | 12.04 | 0.9412 | 0.9418 | 26 | 137.33 | 0.7193 | 0.7193 |
| 6 | 14.98 | 0.9297 | 0.9303 | 27 | 148.21 | 0.7097 | 0.7098 |
| 7 | 18.13 | 0.9183 | 0.9188 | 28 | 159.76 | 0.7002 | 0.7004 |
| 8 | 21.49 | 0.9070 | 0.9074 | 29 | 172.00 | 0.6908 | 0.6910 |
| 9 | 25.08 | 0.8958 | 0.8961 | 30 | 184.98 | 0.6815 | 0.6818 |
| 10 | 28.91 | 0.8847 | 0.8849 | 31 | 198.73 | 0.6722 | 0.6726 |
| 11 | 33.00 | 0.8737 | 0.8737 | 32 | 213.31 | 0.6631 | 0.6635 |
| 12 | 37.36 | 0.8628 | 0.8627 | 33 | 228.76 | 0.6540 | 0.6544 |
| 13 | 42.00 | 0.8520 | 0.8518 | 34 | 245.13 | 0.6450 | 0.6454 |
| 14 | 46.95 | 0.8412 | 0.8409 | 35 | 262.47 | 0.6361 | 0.6365 |
| 15 | 52.91 | 0.8306 | 0.8302 | 36 | 280.83 | 0.6272 | 0.6276 |
| 16 | 57.81 | 0.8200 | 0.8196 | 37 | 300.28 | 0.6185 | 0.6188 |
| 17 | 63.77 | 0.8096 | 0.8091 | 38 | 320.88 | 0.6098 | 0.6100 |
| 18 | 70.11 | 0.7992 | 0.7987 | 39 | 342.68 | 0.6012 | 0.6012 |
| 19 | 76.85 | 0.7889 | 0.7884 | 40 | 365.77 | 0.5927 | 0.5925 |
| 20 | 84.01 | 0.7787 | 0.7783 | 41 | 390.20 | 0.5843 | 0.5834 |
| 21 | 91.62 | 0.7686 | 0.7682 | 42 | 416.06 | 0.5759 | 0.5751 |



Figure 2. Variation in $V(P, T) / V(0, T)$ with pressure for CsCl at different temperatures:
——_ calculated; ....., Decker's data.

Table 4. $V(P, T) / V(0, T)$ as a function of pressure at $25^{\circ} \mathrm{C}$ for sodium chloride. The experimental data are taken from Liu et al (1970).

|  | $V(P, T) / V(0, T)$ |  |
| :--- | :--- | :--- |
| (kbar) | Experimental | Calculated |
| 40 | 0.883 | 0.8829 |
| 78 | 0.819 | 0.8175 |
| 84 | 0.810 | 0.8093 |
| 95 | 0.796 | 0.7951 |
| 102 | 0.788 | 0.7868 |
| 110 | 0.778 | 0.7777 |
| 137 | 0.751 | 0.7505 |
| 161 | 0.731 | 0.7298 |
| 170 | 0.722 | 0.7227 |
| 183 | 0.713 | 0.7130 |
| 190 | 0.708 | 0.7080 |
| 194 | 0.705 | 0.7052 |
| 200 | 0.701 | 0.7011 |
| 202 | 0.699 | 0.6998 |
| 204 | 0.698 | 0.6985 |
| 222 | 0.687 | 0.6870 |
| 232 | 0.680 | 0.6810 |
| 235 | 0.679 | 0.6793 |
| 247 | 0.672 | 0.6724 |
| 268 | 0.660 | 0.6611 |
| 272 | 0.658 | 0.6591 |
| 288 | 0.650 | 0.6511 |
| 290 | 0.649 | 0.6501 |
| 300 | 0.645 | 0.6454 |

The calculations of $\alpha(P, T)$ are carried out for sodium chloride at 300 K in order to compare them with the available experimental data for this solid.
$\alpha(P, T)$ is calculated with the help of equation (12) and taking the values of parameters needed from table 1 . The calculated and the experimental values are reported


Figure 3. Variation in $B_{T}(P, T)$ with pressure for NaCl at different temperatures.


Figure 4. Variation in $B_{T}(P, T)$ with pressure for CsCl at different temperatures.


Figure 5. Variation in $B_{T}^{\prime}(P, T)$ with pressure for NaCl and CsCl at $25^{\circ} \mathrm{C}$.
in table 5. The experimental values in parentheses are taken from Boehler and Kennedy (1980b).

Our calculated values of $\alpha(P, T)$ are closer to the values reported by Boehler and Kennedy (1980b) than to the values given by Spetzler et al (1972). Even then, the agreement between the calculated and the experimental values is good.

Table 5. $B_{T}(P, T)$ and $\alpha(P, T)$ as a function of pressure at 300 K for sodium chloride. The experimental data are taken from Spetzler et al (1972) and the experimental values in parentheses are taken from Boehler and Kennedy (1980b).

|  | $B_{T}(P, T)(\mathrm{kbar})$ |  |  | $\alpha(P, T) \times 10^{-4}(\mathrm{~K})$ |  |
| ---: | :--- | :--- | :--- | :--- | :--- |
| $P$ <br> (kbar) | Calculated | Experimental |  | Calculated | Experimental |
| 0 | 240.14 | 238.41 |  | 1.1752 | $1.1752(1.169)$ |
| 2 | 249.21 | 248.96 |  | 1.1324 | 1.1218 |
| 4 | 258.25 | 259.17 |  | 1.0928 | 1.0737 |
| 5 | 262.77 | - |  | 1.074 | $(1.054)$ |
| 6 | 267.28 | 269.02 |  | 1.0559 | 1.0299 |
| 8 | 276.28 | 278.49 |  | 1.0215 | 0.9899 |
| 10 | 285.26 | 287.55 |  | 0.9893 | $0.9532(0.968)$ |
| 15 | 307.61 | - | 0.917 | $(0.898)$ |  |
| 20 | 329.83 | - | 0.856 | $(0.841)$ |  |
| 25 | 351.90 | - | 0.802 | $(0.796)$ |  |
| 30 | 373.84 | - | 0.756 | $(0.756)$ |  |

Thus, equation (12) can also be used at high pressures and various temperatures to calculate $\alpha(P, T)$ once the values of $B_{T}(P, T)$ become known as a function of pressure and temperature. It may be mentioned here that the calculated values of $\alpha(P, T)$ at 550 and 800 K in the pressure range $0-10 \mathrm{kbar}$ are found to be in agreement with the experimental data (Spetzler et al 1972).

### 3.4. The Anderson-Grüneisen parameter

The physical significance of the Anderson-Grüneisen parameter $\delta_{T}$ has been emphasised by several workers (Anderson 1966, 1967, Chang 1967, Broadhurst and Mopsik 1970, Dass and Kumari 1984).

The parameter is defined as

$$
\begin{equation*}
\delta_{T}(P, T)=-\left\{1 /\left[\alpha(P, T) B_{T}(P, T)\right]\right\}\left[\partial B_{T}(P, T) / \partial T\right]_{P} \tag{13}
\end{equation*}
$$

On the basis of the Grüneisen relation, Chang (1967) expressed $\delta_{T}$ as

$$
\begin{equation*}
\delta_{T}(P, T)=\left[\partial B_{T}(P, T) / \partial P\right]_{T}-1 \tag{14}
\end{equation*}
$$

whereas Dass and Kumari (1984) expressed this parameter as

$$
\begin{equation*}
\delta_{T}(P, T)=\left[\partial B_{T}(P, T) / \partial P\right]_{T} \tag{15}
\end{equation*}
$$

Equations (14) and (15) are derived on the assumptions that $q=0$ and $q=1$, respectively, and also that $C_{V}$ is independent of pressure; here $q$ is the second Grüneisen parameter and is defined in term of Grüneisen parameter $\gamma=\alpha V B_{T} / C_{V}$ as

$$
\begin{equation*}
q=[\partial \ln \gamma / \partial \ln V]_{T} \tag{16}
\end{equation*}
$$

It is appropriate to mention here that equation (15) is certainly better than equation (14) on the grounds that Boehler (1983) have found the value of $q \simeq 1.0$ experimentally. Thus the value of and the variation in $\delta_{T}(P, T)$ with pressure are the same as those for $B_{T}^{\prime}(P, T)$ as reported in figure 5.

## 4. Conclusion

It can be concluded from the discussion given above that the present equation of state is quite successful in representing $V(P, T) / V(0, T)$ behaviour at high pressures and high
temperatures. However, it may be mentioned here that the present results will definitely improve further if the temperature variation of $B_{T}^{\prime}(P, T)$ is also taken into the theory. This will also remove the drawback of the theory that $\delta_{T}(P, T)$ is a temperatureindependent quantity although the adjustable parameters will increase from four to five.

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